



Optimierung und Skalierung von Fluidsystemen

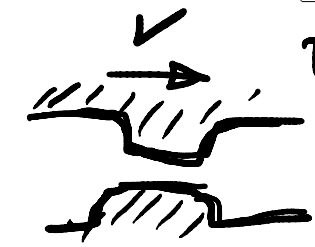
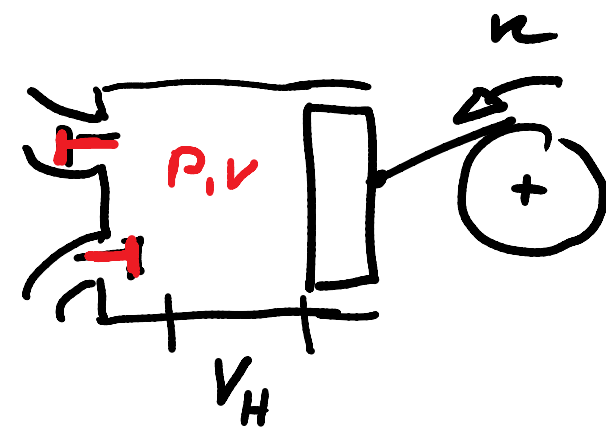
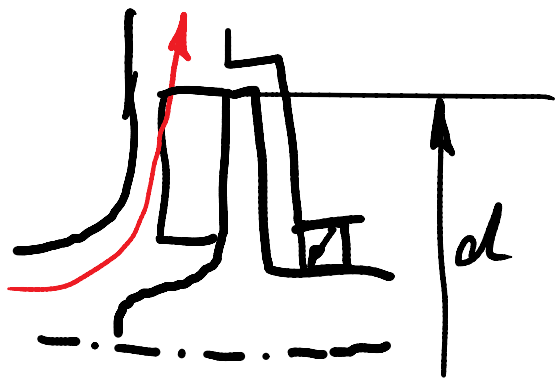
Fluidenergiermaschinen

Modell

Verdrängen
hydrostatische Maschine

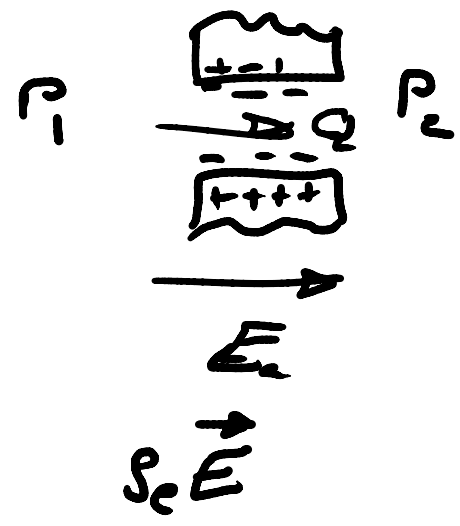
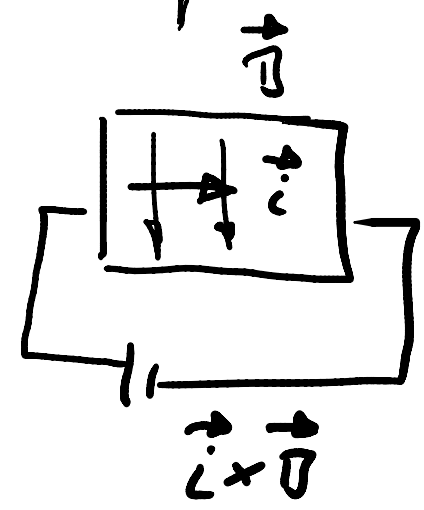
Elektroenergie

Verbrennung
hydrodynamisch



Viskosität

Elektroenergie

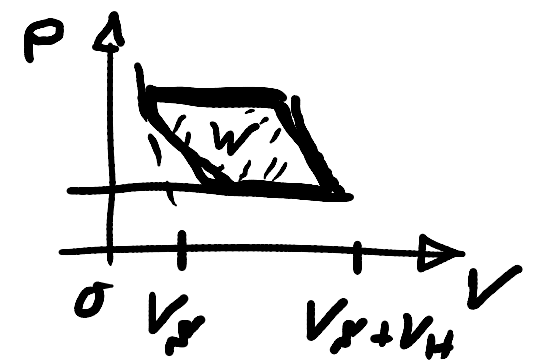


$$dM_2 = dm (T_2 c_{m2} - T_1 c_{m1})$$

$$\frac{\partial}{\partial t} = 0 \quad \text{General Ener 1756}$$

INVEST $\sim d^3$

$$Q_{VH} = 2V_H n$$





Modelliert

Arbeitsm.

$$\Delta P = P_2 - P_1$$

reale Kurve

nicht die Kurve in
eine Gerade m.

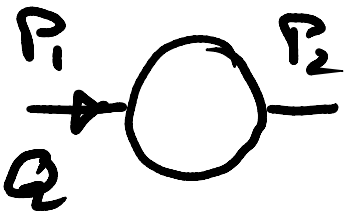
$$\sum P_R = \Delta P Q > 0$$

$$P_R = \sum \Delta P Q < 0$$

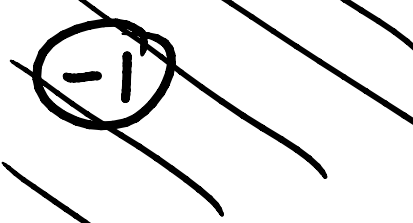
$$\Delta P = \rho g H_T$$

$$Q_{Hl} = n z V_H$$

$$\sum_{\pm 1} = \frac{\Delta P Q}{P_R} = \frac{\Delta P V_H z}{\underbrace{M_z}_{m_H} 2\pi} \cdot \frac{Q}{V_H z h}$$



Wpumpen



Q_{Hl}

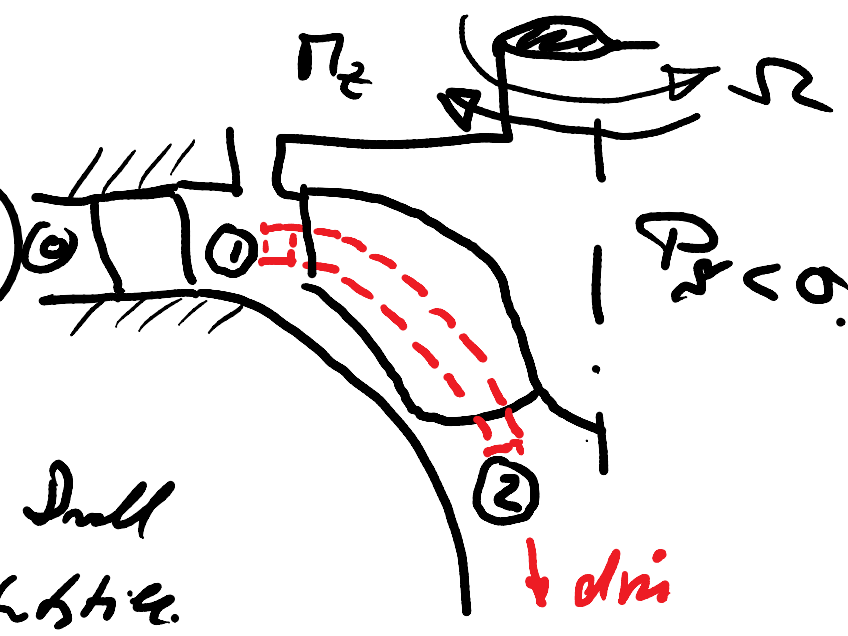


Turbomachine (Turbine, sofern es eine Kraftmaschine ist)



Euler'scher Drehmoment in \vec{e}_2 Punkt

$$\Omega^* \mid dM_2 = d\dot{m} (\tau_2 c_{u2} - \tau_1 c_{u1})$$



$$\tau c_u = (\vec{x} \times \vec{c}) \cdot \vec{e}_2$$

Messspez. Dreh
moment Flussrichtung

$$\vec{x} = r \vec{e}_r + z \vec{e}_z$$

$$\vec{c} = c_r \vec{e}_r + c_u \vec{e}_\varphi + c_z \vec{e}_z$$



$$dP_{\text{S}} = dQ (u_2 c_{u2} - u_1 c_{u1}) \rho$$

[2 2 177]

1. NS:

$$dP_{\text{S}} + dQ = d\dot{m} (h_{t2} - h_{t1})$$

± 1

$$\sum dP_{\text{S}} = dQ (P_{t2} - P_{t1})$$

\parallel
 $\sim P_2 - P_1$

\equiv

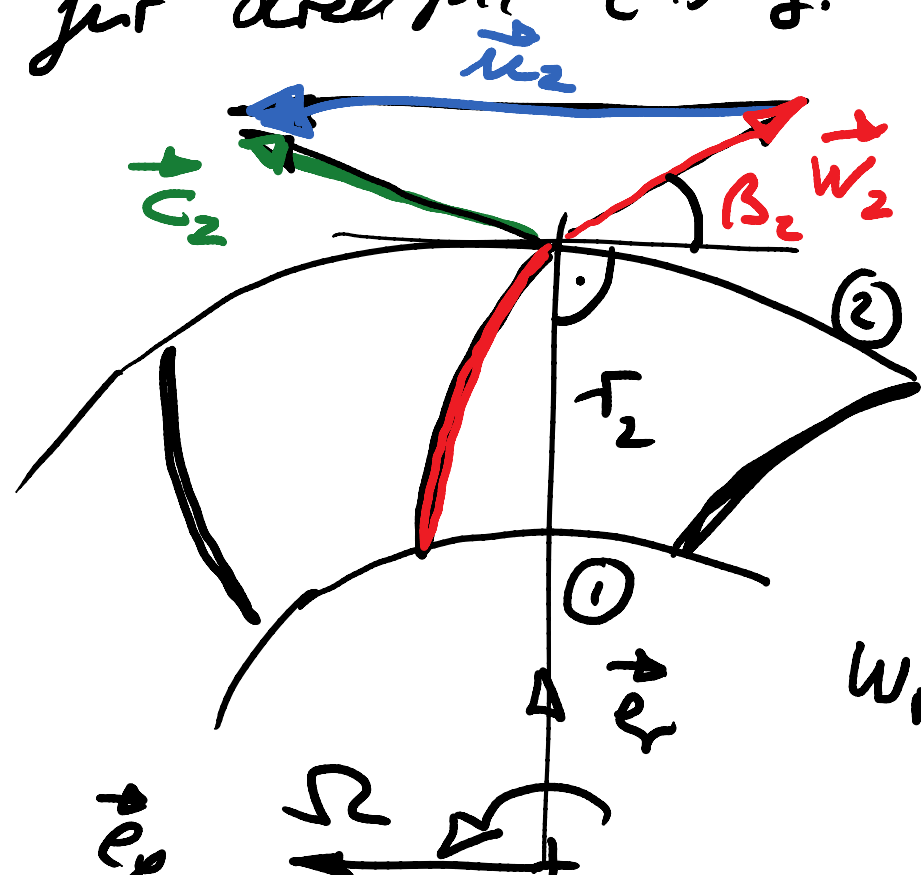
$$\rho = \rho_1 = \rho_2$$
$$dQ \equiv 0$$



$$\int \frac{P_{t2} - P_{t1}}{\rho} = \int \left(\underbrace{M_2}_{\equiv \sigma} c_{u2} - \underbrace{M_1}_{\equiv \sigma} c_{u1} \right)$$

$$c_{u2} = \vec{c} \cdot \vec{e}_\varphi = (\vec{u} + \vec{w}) \cdot \vec{e}_\varphi$$

$c_{u1} \equiv 0$ für axiale Zust. $= \Omega r_2 - w_{r2} \cot \beta_2$



$$\vec{c} = \vec{u} + \vec{w} (+ \vec{u})$$

↑
↑
↑
u-feld
Relativ.
Führung.

$$w_{r2} \equiv \frac{Q}{2\pi r_2 b}$$



$$\frac{P_{t2} - P_{t1}}{\rho} = z^{\pm 1} \left((\tau_2 \Omega)^2 - \tau_2 \Omega \frac{Q}{2\pi \tau_2 b} c_f \beta_2 \right)$$

Umschreiben in Abstraktion, da

$$c_{k1} = 0$$

$$\frac{2}{(\tau_2 \Omega)^2}$$

$$\frac{P_{t2} - P_{t1}}{\rho u_2^2} = z^{\pm 1} \left(2 - 2 \underbrace{\frac{Q}{2\pi \tau_2^2 b \Omega}}_{\varphi} c_f \beta_2 \right)$$

$$= \psi$$



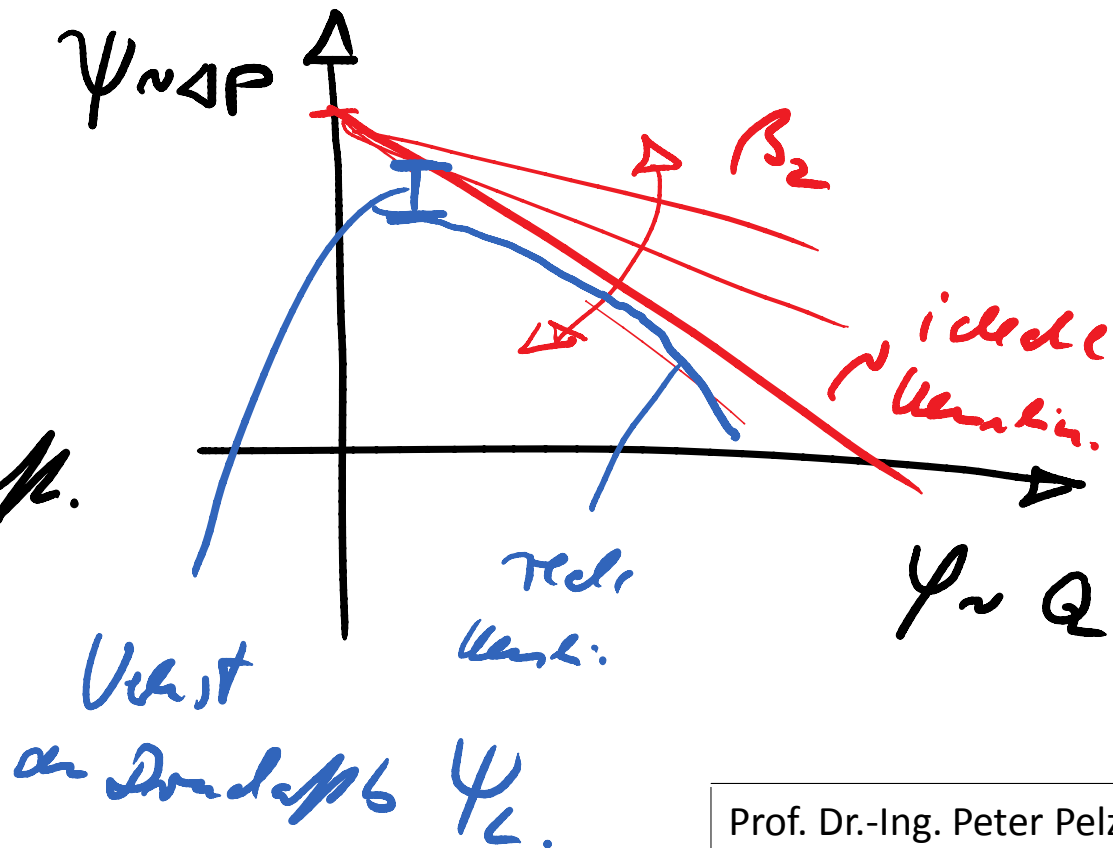
$$\psi = 2 z^{\pm 1} (1 - c \delta \rho_2 \psi)$$

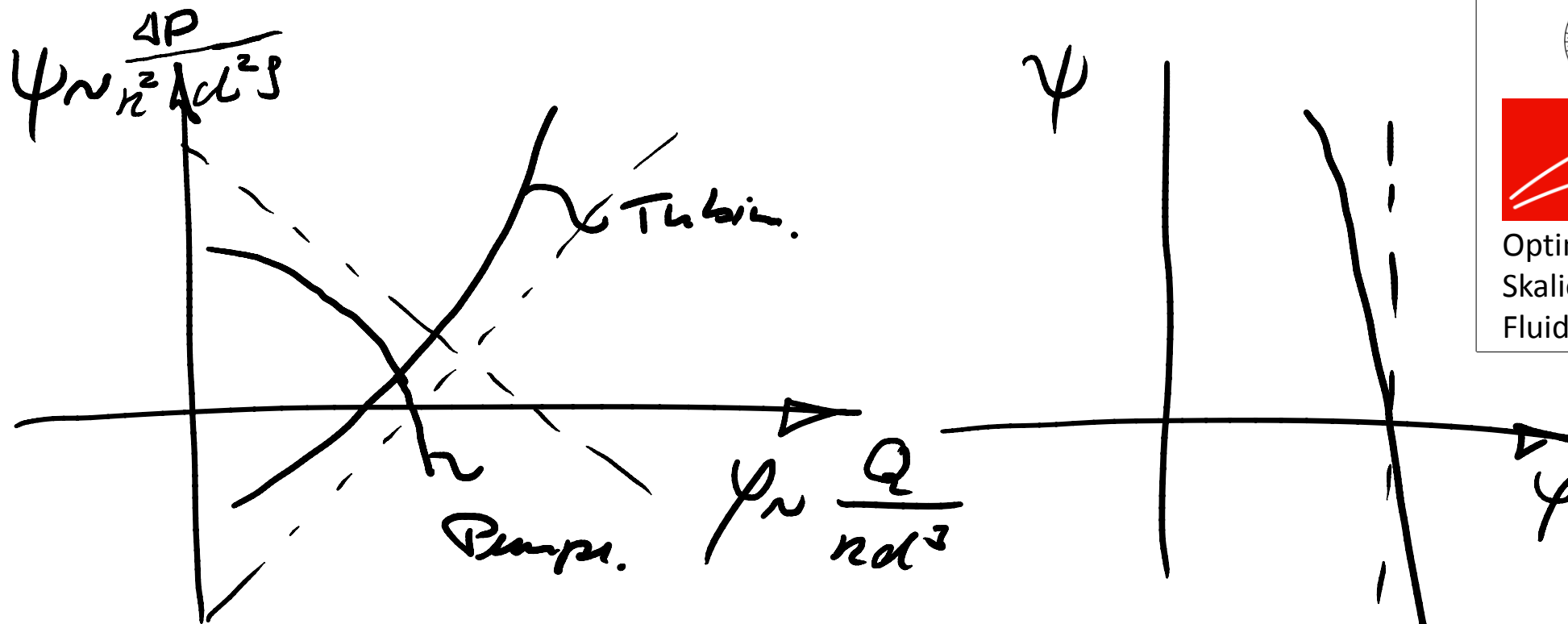
$$\psi = \frac{2 \Delta P}{\rho u_2^2}$$

Druckk. $\psi \sim \Delta P$

$$\psi = \frac{Q}{2 \pi r_2^2 b \Omega}$$

Druckk. $\psi \sim Q$





Turbomach.

$$\pm \frac{\psi}{\hat{\psi}} = z^{\pm 1} \left(1 - \frac{Q}{\hat{Q}} \right)$$

+1 Arbeit

-1 Turbine

Hydrostatische Maschine.

$$\psi = z^{\pm 1} \hat{\psi}$$

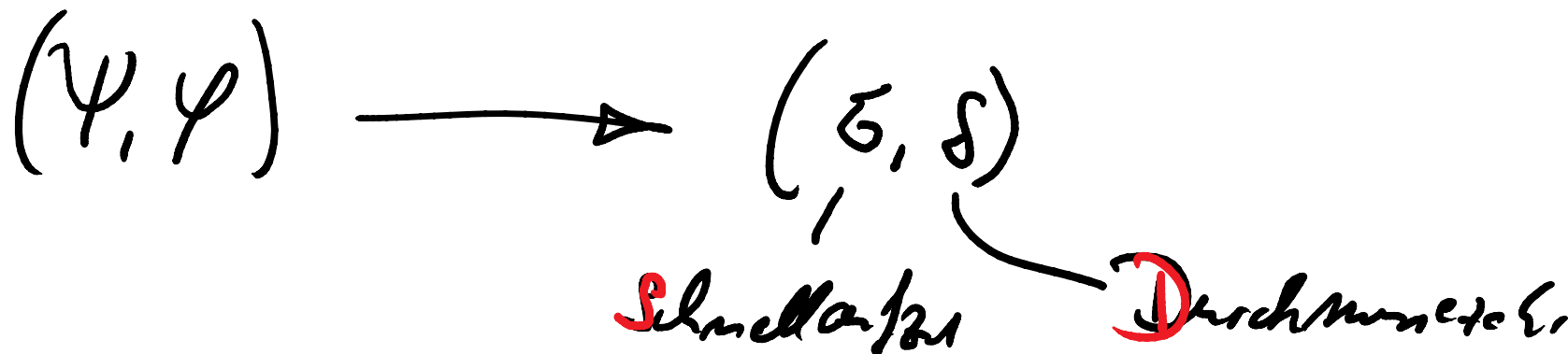


$$g H_T = g \frac{2}{5} H_{\text{M}} \quad \checkmark$$

$$x \in \mathbb{R} \leadsto d^3 \quad \checkmark$$

λ klein, desto besser!

Drehzahl \sim Nutzfrequenz \checkmark



$$\psi = z \hat{\psi} \left(1 - \frac{y}{\delta}\right)$$

$$\psi = \frac{1}{g^2 \delta^2}$$

$$\varphi = \frac{1}{g^3 \delta}$$

Schnelllaufzeit

$$\delta := 2 \sqrt{\pi} \left(2g H_T\right)^{-\frac{3}{4}} Q^{\frac{1}{2}} \quad \alpha \neq f_\alpha(\alpha)$$

Keller 1934: Diss. ETH Zürich.

Deutsches Institut

$$\delta := \frac{\sqrt{\pi}}{2} \left(2g H_T\right)^{\frac{1}{4}} Q^{-\frac{1}{2}}$$

$$\alpha \neq f_\alpha(u)$$

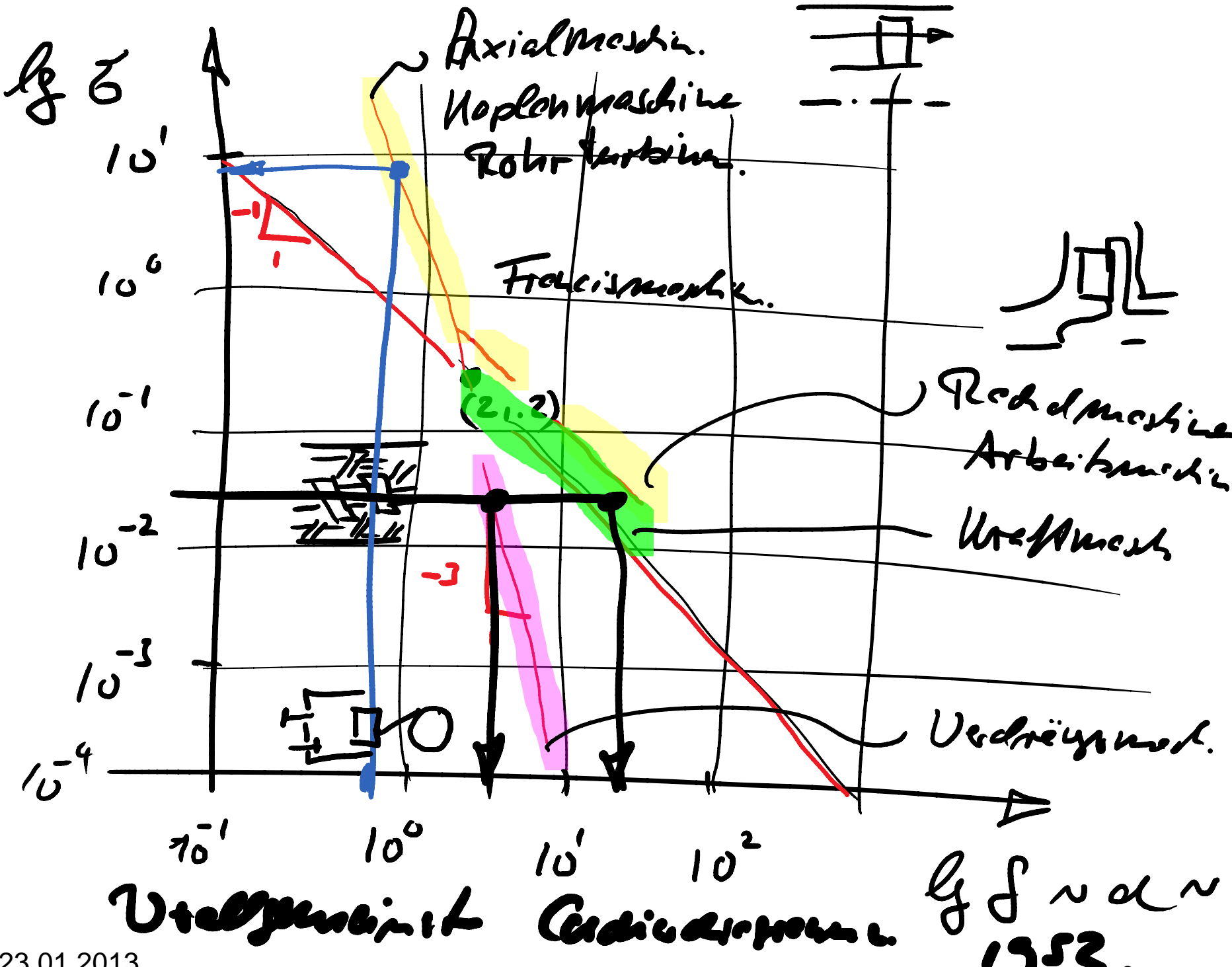


TECHNISCHE
UNIVERSITÄT
DARMSTADT



FLUID
SYSTEM
TECHNIK
Optimierung und
Skalierung von
Fluidsystemen

Prof. Dr.-Ing. Peter Pelz
Wintersemester 2012/13
Vorlesung 9 F 121



⊕ schöne
Angebot

⊕ Einfach
Nachweise

Otto Corolier

VDI

1952



TECHNISCHE
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