

$$\left[\frac{D\vec{I}}{Dt} \right]_{\vec{I}} = \left[\frac{D\vec{I}}{Dt} \right]_{\vec{B}} + \vec{\Omega} \times \vec{I}.$$



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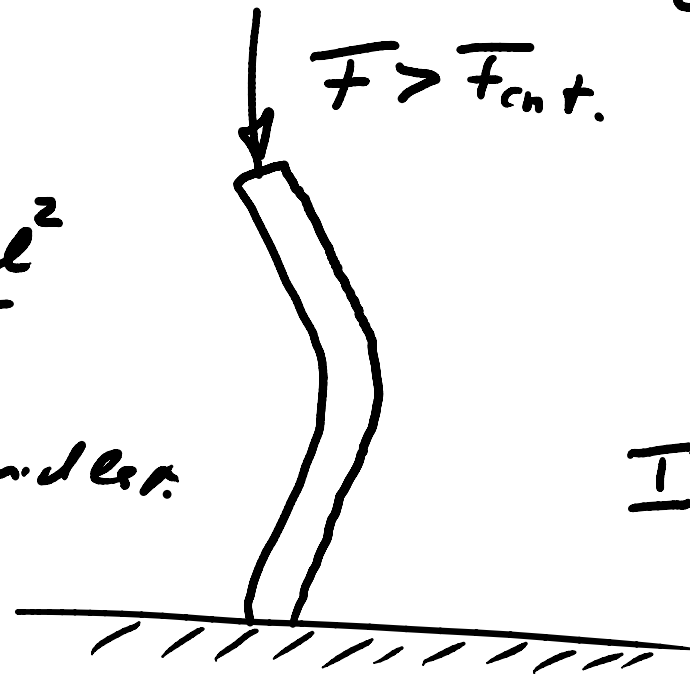
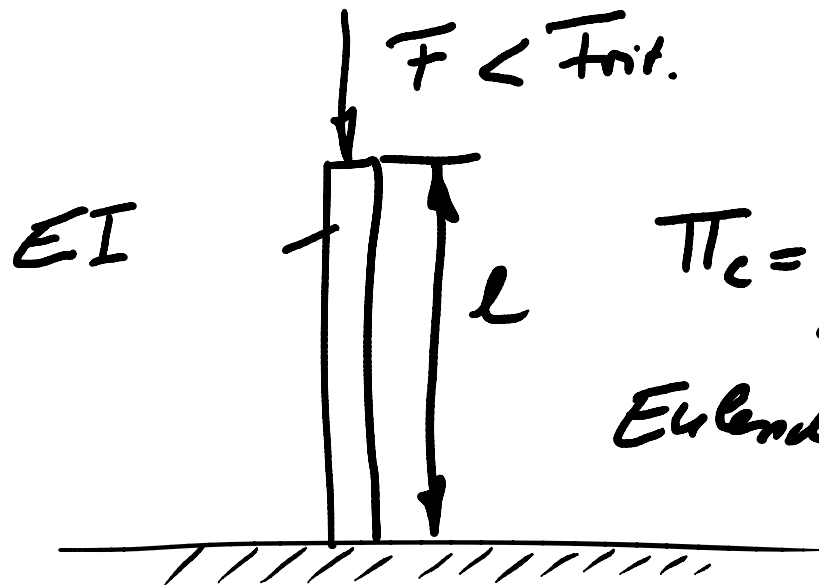


Technische
Fluidsysteme



stabil $\pi < \pi_c$

instabil. $\pi > \pi_c$



$$\pi_c = \frac{F_c l^2}{EI}$$

Euler's number

$$I = \int_{\Omega} \xi^2 d\Omega$$

$$F_{crit} = f_{crit}(l, EI)$$

{ }

Einheit

Eigenwert.

$$\{EI\} = Nm^2$$

$$[EI] = FL^2$$

[]

Größenart.

$$\{F_{crit}\} = N; [F_{crit}] = F$$

$$\{l\} = m; [l] = L$$



$$F_{crit} = \sqrt[4]{L (EI)}$$

N

10 m
= 10³ cm

Nm²

Übersatz:

1. dimensionshomogener
Zusammenhang.

↓ Produktfkt.

2. Gewicht wird
nun mit Maßzahl!

$$F_{crit} = \sqrt[4]{L \left(\frac{EI}{l^2}, \cancel{EI} \right)}$$

N

N

~~Nm²~~

3. Physikalisch-technische
Zusammenhänge sind
invariant gegenüber
Änderung des
Basiswertesystems. } Bridgman
Postulat.

↓

Bridgman-Postulat

"Absolute Bedeutung" "relativer Größen"

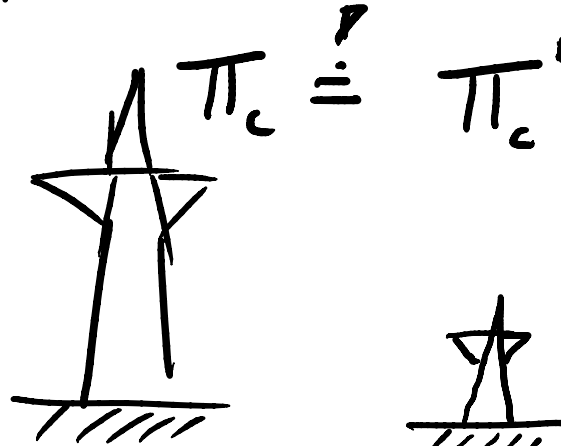
$$F_{crit} = f_n(l, EI)$$

$$F_{crit} = f_n\left(\frac{EI}{l^2}, \cancel{EI}\right)$$

$$\Pi_c = \frac{F_{crit} l^2}{EI} = f_n\left(\frac{\cancel{EI}}{\cancel{l^2}}\right) = const$$

dimensionlose
Konstante

dimensionalen Produkte.



$\Pi_c \doteq \Pi_c'$ geometrische
Ähnlichkeit.
↳ gleiche Gestalt.



physikalische
Ähnlichkeit.

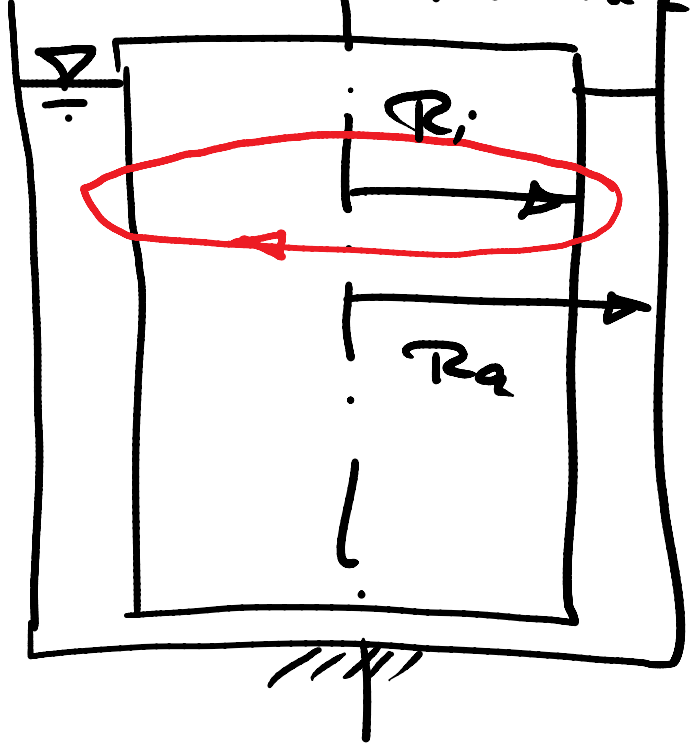
↳





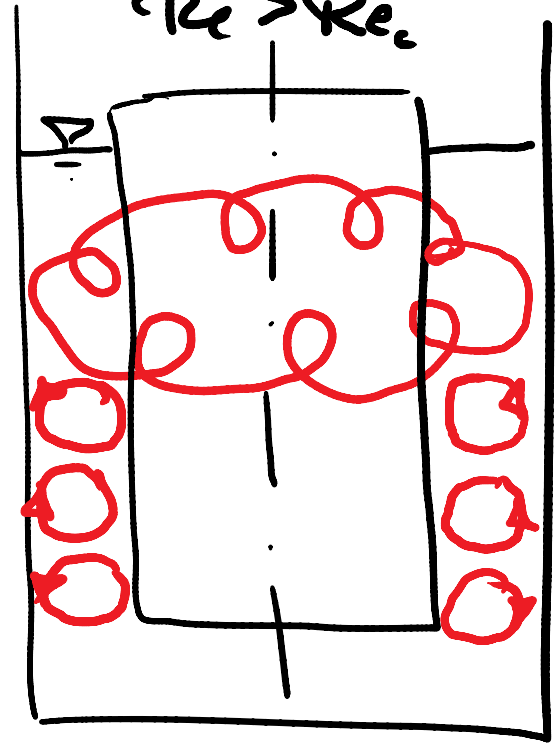
$$\Omega < \Omega_c$$

$$Re < Re_c$$



$$\Omega > \Omega_c$$

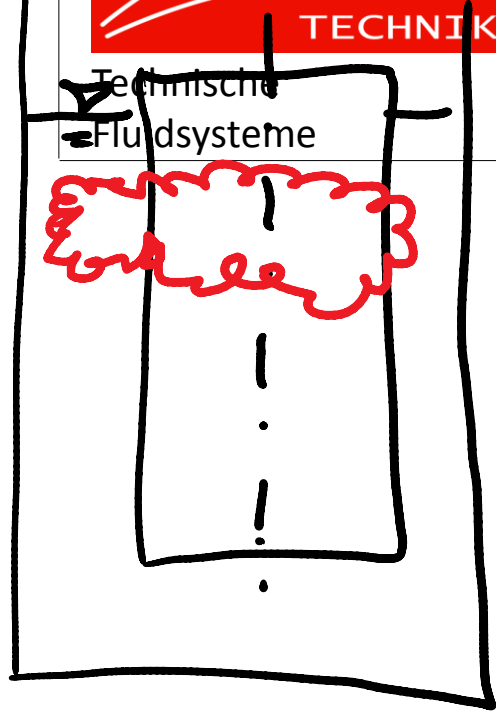
$$Re > Re_c$$



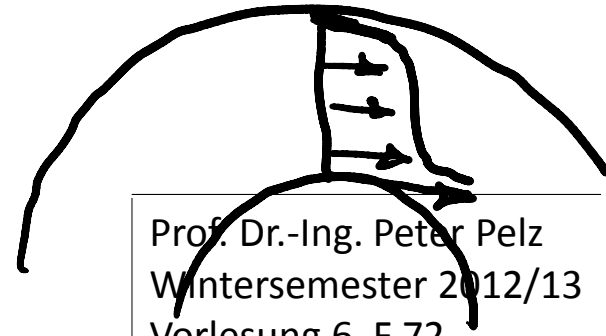
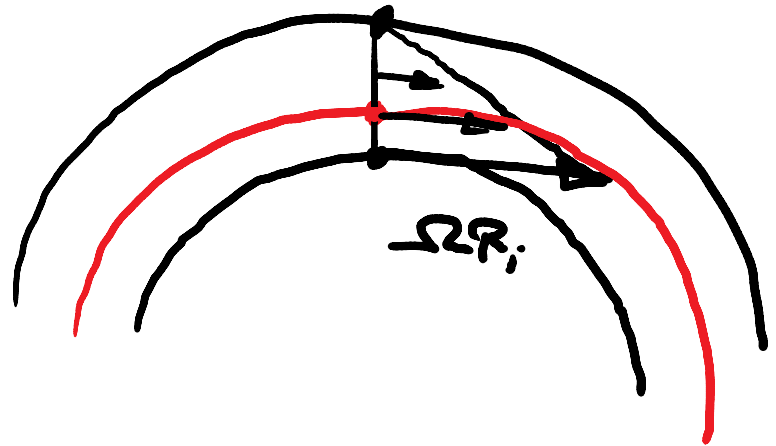
G.I.
Taylor
Vortex

$$\Omega \gg \Omega_c$$

$$Re \gg Re_c$$



Türmlinge und
zeitliche Strukturen
bilden sich ab



Der Weg in die Turbulenz führt
über Verzweige (Instabilität).



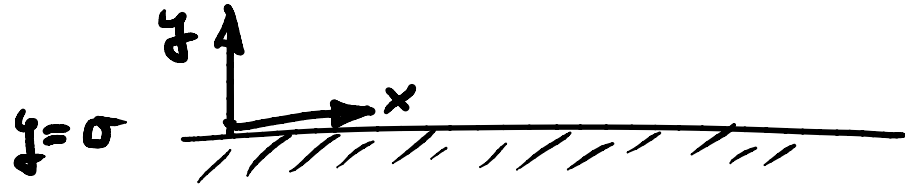
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Couette-Strömung



- im zeitlichen Mittel quasi-stationäre Strömung

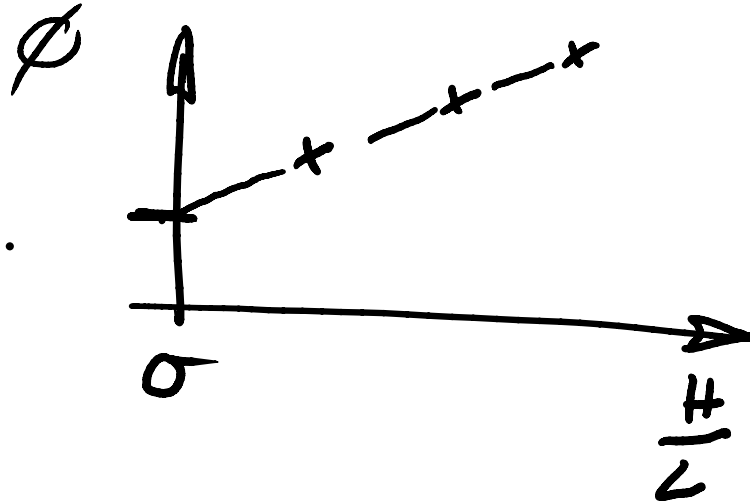
$$\frac{\partial}{\partial t} \equiv 0$$

- unendlich ausgedehnte Platte \rightarrow keine Randeffekte.

Hinweis: Wenn Randeffekte zu
groß sind, soll die
des Schlechthochfrequenz

$$\frac{L}{\lambda}$$

Extrapolation:



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Vorlesung 6 F 75



$$\rho \frac{D\vec{u}}{Dt} = \nabla \cdot \vec{T} + \vec{f} \quad \left| \begin{array}{l} \cdot \vec{e}_x \\ \cdot \vec{e}_y \end{array} \right.$$

$$0 = \rho \frac{Du}{Dt} = (\nabla \cdot \vec{T}) \cdot \vec{e}_x + f_x$$

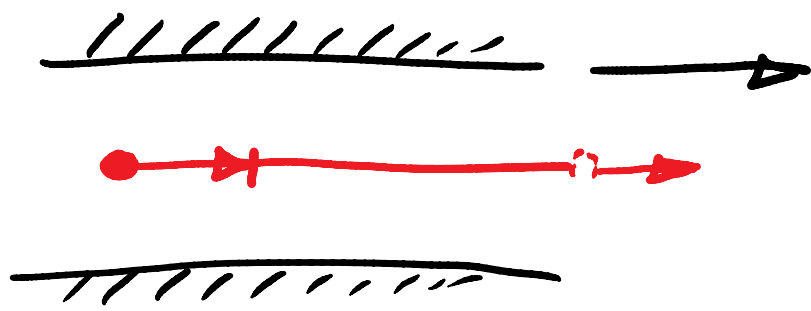
$$0 = \rho \frac{Dv}{Dt} = (\nabla \cdot \vec{T}) \cdot \vec{e}_y + f_y$$

- laminares Ström.

- kein Volumenwert

$$\vec{f} \equiv 0$$

- $\vec{u} = u \vec{e}_x$



$$\nabla \cdot \vec{T} = 0; \quad v \equiv 0$$

Bewert.



$$\underline{\underline{\tau}} = \tau_{xx} \vec{e}_x \vec{e}_x + \tau_{xy} \vec{e}_x \vec{e}_y + \tau_{yx} \vec{e}_y \vec{e}_x + \tau_{yy} \vec{e}_y \vec{e}_y$$

$$\tau_{xx} = -p + 2\eta \frac{\partial u}{\partial x}$$

Viskose Normalspannung.

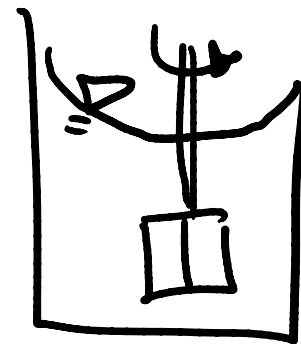
$$\tau_{xy} = \eta \frac{\partial u}{\partial y} = \tau_{yx}$$

$$\tau_{yy} = -p + 2\eta \frac{\partial v}{\partial y}$$

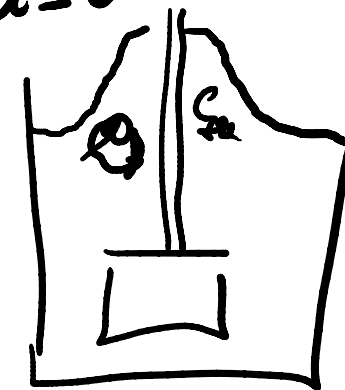
$$v \equiv \sigma$$

Kontin. $\frac{D\rho}{Dt} + \rho \nabla \cdot \vec{u} = 0.$

$\frac{D\rho}{Dt} \equiv 0$ Inkompressibel. $\rightarrow \nabla \cdot \vec{u} = 0$



Newton.



Nicht-Newtonian.

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

Normalspannungskontinuität

Verfärbung etc.

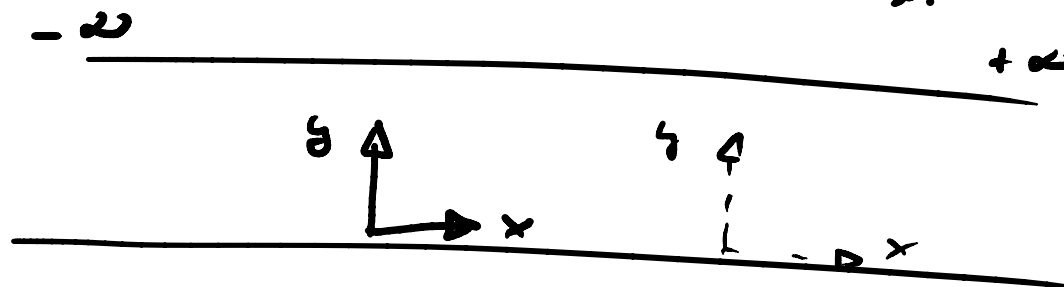


$$\sigma = \frac{d}{dy}(\tau_{xy})$$

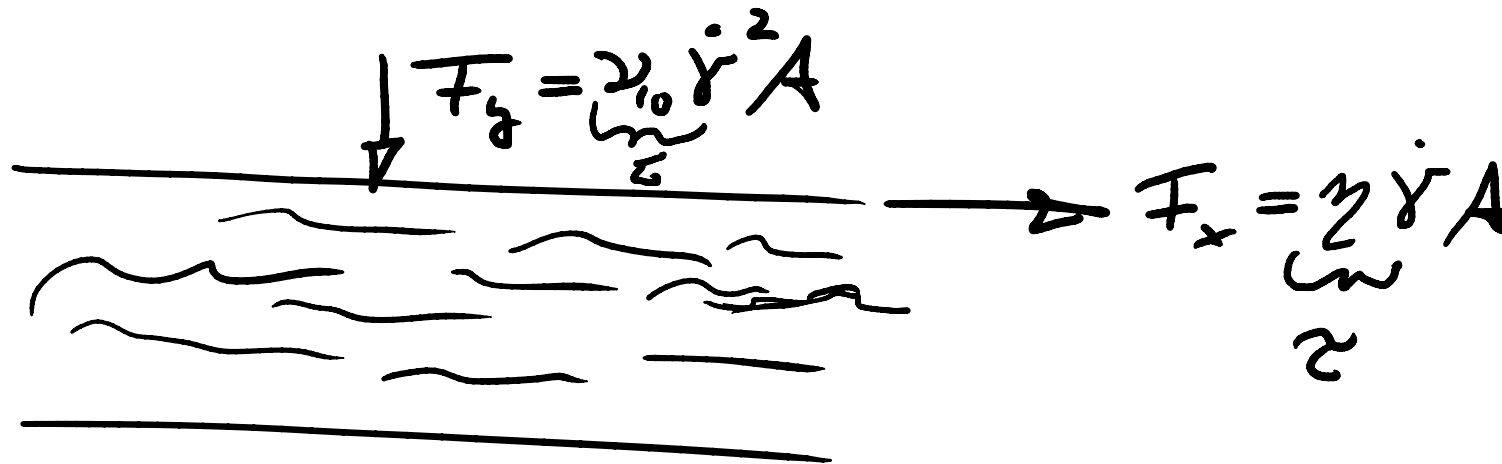
$$v \equiv \sigma$$

$$\left. \begin{aligned} v(y=0) &= \sigma \\ v(y=h) &= \sigma \end{aligned} \right\} \begin{array}{l} \text{Keilström} \\ \text{Rohrström.} \end{array}$$

$$\cancel{\frac{\partial v}{\partial x}} + \frac{\partial v}{\partial y} = 0. \quad \leadsto \quad v = \text{const} + \int f(x) dy = C_1$$



$$\frac{\partial v}{\partial x} = 0 \quad \text{aus Symmetrie}$$



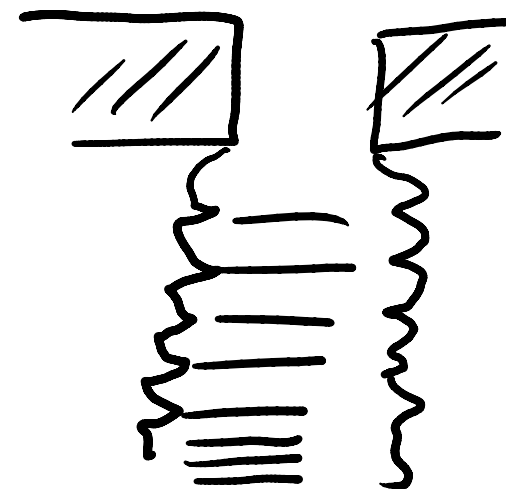
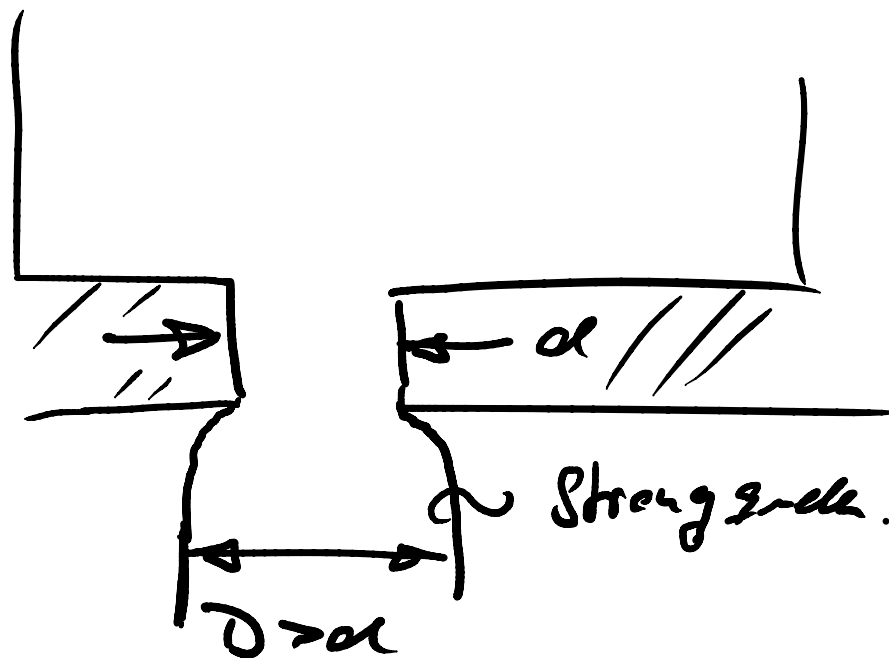
ρ_0 Molekulgewicht.

$$\uparrow We = \frac{\sigma_E}{\rho \dot{\gamma}} = \frac{\rho_0 \dot{\gamma}^2}{\rho \dot{\gamma}}$$

$Uc > U_{c,c}$ viskoelastisch
Turbulenz.
Schmelzen.

$$Re = \frac{\sigma_T}{\rho \dot{\gamma}} = \frac{\rho \mu^2}{\rho \dot{\gamma}}$$

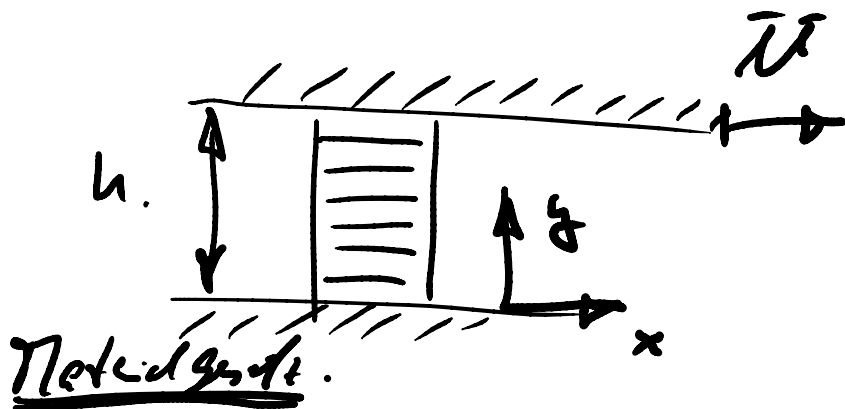
$Re > Re_c$ turbulenz



Bewegungsgleichung:

$$\sigma = \frac{d}{dy}(\tau_{xy})$$

$$\tau_{xy} = \text{const.} = \tau_w \quad \text{Wand Schubspannung.}$$



$$\mu(y) = \frac{\tau_w}{\eta} y = \bar{\mu} \frac{y}{h}$$

$$\tau_{xy} = \eta \frac{d\mu}{dy}$$

$$\tau_w = \eta \frac{d\mu}{dy} \Rightarrow \frac{\tau_w}{\eta} y + \text{const.} = \mu(y) \quad \parallel \sigma \text{ Notwend.}$$



Drukgetriebene Ström. $\frac{\partial \sigma}{\partial x} = \sigma$

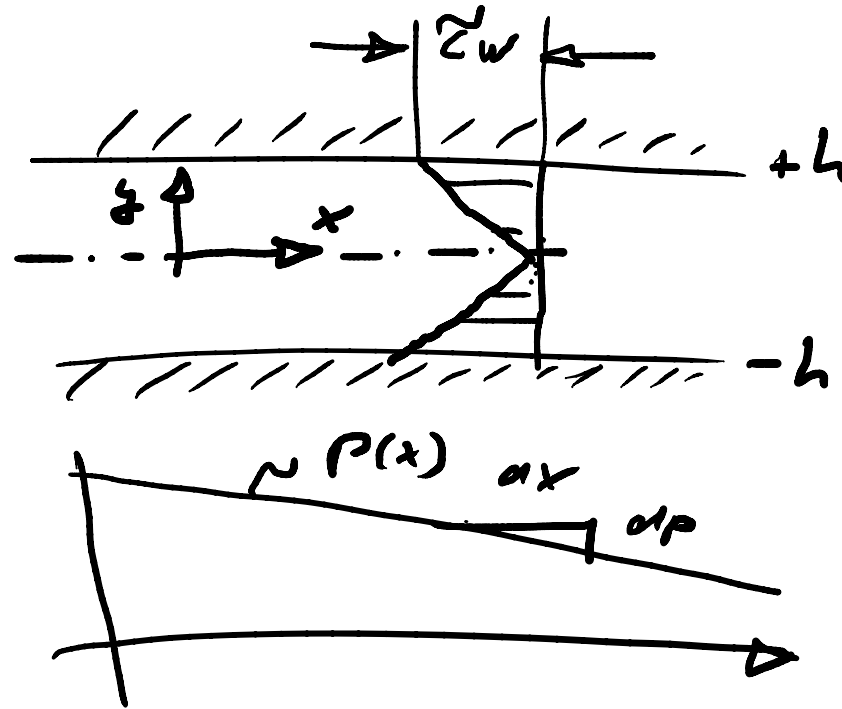
$$\sigma = -\frac{dp}{dx} + \frac{d}{dy}(\tau)$$

$$\frac{dp}{dx} y + \text{const} = \tau(y)$$

//
 σ aus
 Symmetrieprin.

Schubspannung an der Wand

$$-\frac{dp}{dx} h = \tau_w$$



$$\frac{\tau}{\tau_w} = -\frac{y}{h}$$

für Newtonsch. Rheol.

$$\tau = \eta \frac{du}{dy}$$

$$u = \text{const} - \frac{1}{2} \frac{y^2}{h} \frac{\tau_w}{\eta}$$





$$u(h) = 0 \quad \text{Nothbedingung.}$$

$$\hookrightarrow \text{const} = \frac{1}{2} h \frac{z_w}{z}$$

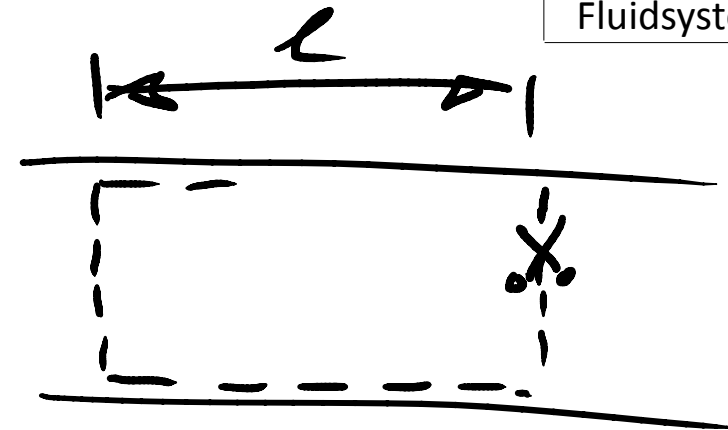
$$u(y) = \frac{1}{2} \frac{z_w h}{z} \left(1 - \left(\frac{y}{h} \right)^2 \right).$$

u_{max}

Mittleren Strömungsgeschw.

$$\bar{u} = \frac{1}{h} \int_0^h u(y) dy = \frac{1}{h} \frac{z_w h}{z} \frac{2}{3} = \frac{2}{3} \frac{z_w h}{z}$$

Widerstandsbezug



$$\cancel{p} 2h - \left(\cancel{p} + \frac{dP}{dx} L \right) 2h = \cancel{z} \cancel{z}_w$$

ΔP

$$z_w = - \frac{dP}{dx} L$$